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Mixing Characteristics of Directly Opposed Rows of Jets Injected Normal to a Crossflow in a Rectangular Duct

D.S. Liscinsky and B. True
*United Technologies Research Center
East Hartford, Connecticut*

and

J.D. Holdeman
*Lewis Research Center
Cleveland, Ohio*

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D.S. Liscinsky* and B. True**
United Technologies Research Center
East Hartford, CT 06108

J.D. Holdeman†
NASA Lewis Research Center
Cleveland, OH 44135

Abstract

An experimental investigation of the mixing of non-reacting opposed rows of inline jets injected perpendicular to a uniform crossflow has been conducted in a rectangular duct. Planar Mie-scattering was used to measure the time-average concentration distribution of the jet fluid in planes perpendicular to the duct axis.

Orifice configurations with geometric blockages ranging from 0.59 to 0.89 had similar mixing performance when compared at one-half duct height downstream of injection. Blockage was varied by changing the orifice aspect ratio from 1-to-1 to 1-to-1.5 while maintaining orifice spacing-to-duct height (S/H) at 0.425, jet-to-mainstream mass flow ratio (MR) at 2.0, and jet-to-mainstream momentum-flux ratio (J) at 48. The result indicates that the design correlating expression (at $MR = 2$) for optimum inline mixing of $2.5 \approx (S/H)\sqrt{J}$ is independent of the web between adjacent orifices and therefore independent of orifice width. Experimental and numerical results for an orifice aspect ratio 1-to-1 case were in good agreement.

The results of a comparison of inline 45° slanted slot and round orifice configurations indicate that in order to obtain equivalent mean concentration distributions at the same J it is necessary to use a smaller S/H for the round orifice configuration. Conclusions about the performance of various orifice shapes can only be obtained from comparison of optimized configurations.

Inline jets with different momentum-flux ratios on opposite sides were compared at a constant mass flow ratio. The orifice spacing chosen was previously found to be an optimum configuration when opposing values of J were equal and also an optimum for single side injection. Experimental and empirical results were in good agreement.

Nomenclature

Ar	jet-to-mainstream area ratio = A_j / A_m
B	blockage = y projection / S
C	$(S/H) * \sqrt{J}$ (see Eq. 1)
c_{avg}	$(m_j / m_m) / (1 + m_j / m_m) = \theta_{EB}^{17}$
C_d	orifice discharge coefficient
DR	jet-to-mainstream density ratio = $\rho_j / \rho_m = 1.0$
D	orifice diameter
H	duct height at injection plane = 2 in
J	jet-to-mainstream momentum-flux ratio = $(\rho_j V_j^2) / (\rho_m V_m^2)$
MR	jet-to-mainstream mass flow ratio = m_j / m_m
S	spacing between corresponding points on adjacent orifices
U_s	spatial unmixedness parameter (see Eq. 2)
V_j	jet velocity = $m_j / (\rho_j A_j C_d)$
V_m	mainstream velocity = 10 ft/s
x	downstream coordinate, $x = 0$ at the leading edge of the orifice
y	cross-stream coordinate

Introduction

Rapid mixing of two steady flows is essential in numerous technology areas, including aeropropulsion, chemical processing, and effluent control. Injection of jets perpendicular to a crossflow has proven to be an effective mixing technique for many of these applications. For example, gas turbine combustion chambers rely on crossflow mixing in the dilution zone to provide a uniformly mixed discharge to the turbine.

Crossflow mixing has recently been proposed as a technique which will provide the rapid mixing required in a propulsion system that has low emissions. The Rich-burn/Quick-mix/Lean-burn (RQL) combustor concept uses axially staged burning zones to avoid stoichiometric mixtures in order to minimize production of oxides of nitrogen (NO_x) while maintaining a high level of combustor efficiency. The quick-mix section is a key technology for this combustor to achieve low emissions¹. Evaluation and enhancement of the performance of the mixing section for this combustor concept has been the subject of many recent experimental and numerical studies of crossflow mixing²⁻¹⁶. The present investigation further addresses the design of this section.

* Research Scientist, Member AIAA

** Senior Laboratory Technician

† Senior Research Engineer, Associate Fellow AIAA

Background

The study of jet mixing in gas turbine combustor dilution zones is generally motivated by concern for turbine durability. Mixing performance in the dilution zone is determined by jet penetration and use of the "optimum" number of jets. The design is satisfactory when a uniform mean temperature distribution is achieved at the exit of the combustor¹⁷⁻¹⁹. Holdeman¹⁷ has shown that the most important design parameters are (1) jet-to-mainstream momentum-flux ratio (J) and (2) orifice spacing-to-duct height ratio (S/H) and that optimum mixing performance is achieved when the product of the orifice spacing and the square root of the momentum-flux ratio are a constant:

$$C = (S/H) \sqrt{J} \quad (1)$$

The value of this constant, C , has been determined empirically over a range of J for orifices with spacing-to-diameter ratios (S/D) ≥ 2 , and $MR \leq 0.5$. Optimum mixing was obtained when $C = 2.5$ for single-side injection, 1.25 for opposed rows of inline jets, and 5.0 for opposed rows of staggered jets.

In the RQL combustor, the design of the mixer is constrained by the need for rapid addition of a large quantity of air at a $\Delta P < 4\%$. While conventional dilution zones typically have jet-to-mainstream mass flow ratios (MR) ≤ 0.5 and may introduce the mass over a length of several combustor heights, the RQL mixer requires a mass addition of $MR \geq 2$ in a length that is less than half a duct height. Designs which achieve this mass addition therefore have high jet-to-duct area ratios compared to conventional dilution zones, the result being large orifices which are closely spaced ($S/D \leq 2$). Directly opposed inline orifices provide the largest mass addition per orifice length of any geometric configuration and therefore recent experimental and numerical studies have concentrated on this orifice configuration for the RQL application. In this investigation, three design considerations for inline orifices are explored: (1) web between adjacent orifices, (2) orifice shape, and (3) jets with different momentum-flux ratios on opposite sides.

Experimental

Figure 1 is a schematic representation of the apparatus. The apparatus consists of 3 parallel contiguous ducts of rectangular cross section, simulating a sector of an annular combustor. Sector width is 12 inches. The inner duct height (H) is variable, but was set at 2 inches for the reported experiments. The outer ducts (shrouds), which supply the injectant gas, are 1 inch in height. These are separated from the inner duct by removable, 0.12 inch thick flat plates. The injectant is fed from the shrouds to the inner duct through orifices of various sizes and shapes that are machined into the plates. Mass flow to each of the 3 ducts is controlled independently using venturi flowmeters. The maximum variation in the mean approach velocity of the mainstream flow was 6% with a turbulence level of 1.3%. All tests were conducted at unity density ratio.

Planar digital imaging was used to optically measure concentration distributions in planes perpendicular to the duct axis, starting at the leading-edge of the orifice and continuing downstream to a location equal to the duct height. The Mie scattering technique²⁰ is applied by marking the jet flow with an oil aerosol (μm sized particles). A light sheet (0.02 inch thick) is created using a 2W argon-ion laser and a rotating mirror. The flow field is illuminated by passing the light sheet through a window in the side wall of the test section. An image intensified thermo-electrically cooled CCD camera, located inside the duct 2.5 ft downstream of the orifice centerline, is focused on the illuminated plane (end-on view). The camera is programmed to make exposures coincident with the sweep of the beam through the flow field. The image is digitized and sent to a computer for storage. The scattered light intensity is proportional to the number of particles in the measurement volume. If only one of two streams is marked (in this study the jet fluid), the light intensity of the undiluted marked fluid represents mole fraction unity.

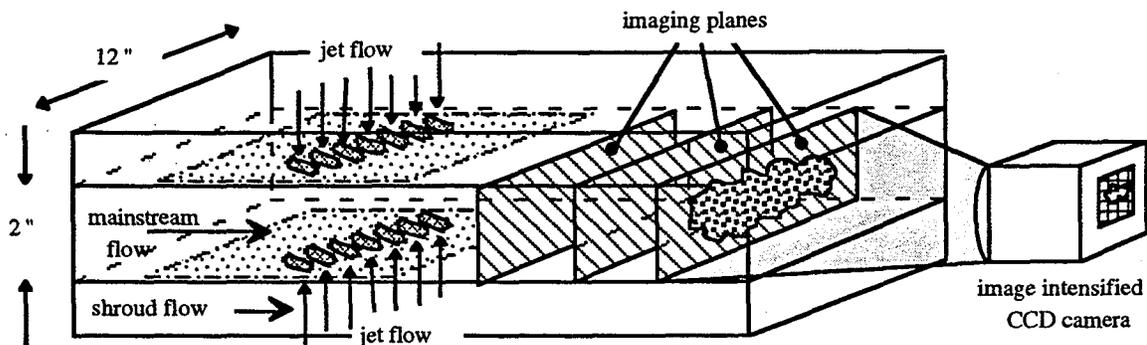


Figure 1: Experimental Configuration used to Measure Planar Concentration Distributions

Analysis

Spatial unmixedness (U_s) is a parameter that quantifies the unmixedness of a distribution, and discussed in detail by the authors in Ref. 7., is defined as:

$$U_s = \frac{C_{var}}{C_{avg}(1 - C_{avg})} \quad (2)$$

where,

$$C_{var} = \frac{1}{m} \sum_{i=1}^m (\bar{C}_i - C_{avg})^2$$

= spatial concentration variance

m = number of pixels in the distribution

\bar{C}_i = time-average concentration at a pixel

C_{avg} = fully mixed concentration = $m_j / (m_j + m_m)$

$C_{avg}(1 - C_{avg})$ = maximum concentration variance
= 0.221 for MR = 2.0

Normalization by $C_{avg}(1 - C_{avg})$ allows comparison of systems of different C_{avg} (different MR) and bounds U_s between 0 and 1. $U_s = 0$ corresponds to a perfectly mixed system, and $U_s = 1$ a perfectly segregated system.

Results and Discussion

Effect of Blockage

The general inverse relationship of J and S/H (Eq. 1) has been shown² to apply when extended to RQL conditions of MR = 2 and S/D ≤ 2. However at those conditions, the proportionality constant, C, has been found, both experimentally⁷ and numerically^{2&6}, to be ≈ 2.5, compared to a value of 1.25 which was reported¹⁷ at S/D ≥ 2. To determine whether C is a function of orifice width, a set of "optimized" orifices with varying geometric blockages (B) were investigated. Rectangularly shaped orifices were used in order to maintain MR = 2.0 and S/H = 0.425 for all configurations. (Blockage cannot be varied at constant MR and S/H using circular orifices).

The effect of varying blockage from 0.59 to 1.0 was investigated by testing the 7 orifice plate configurations shown in Table 1. The first 6 configurations were designed to be optimum inline mixing configurations based on the results of a numerical parametric investigation of aspect ratio and orifice spacing by Bain, Smith and Holdeman². In that numerical study, aspect ratio and orifice shape were found to have little

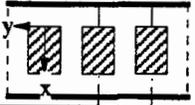
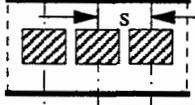
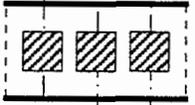
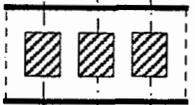
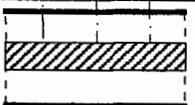
Plate #	Aspect Ratio	Configuration	Width x Length (Δy " x Δx ")	Area Ratio (A_j / A_m)	Design Cd (*)	Blockage †
1	1-to-1.5		0.502 x 0.752	0.444	0.75 (0.66)	0.59
2	1-to-1.25		0.550 x 0.687	0.444	0.75 (0.64)	0.65
3	1-to-1		0.614 x 0.614	0.444	0.75 (0.65)	0.72
4	1-to-1.25		0.687 x 0.550	0.444	0.75 (0.62)	0.81
5	1-to-1.5		0.752 x 0.502	0.444	0.75 (0.62)	0.89
6	1-to-1		0.695 x 0.695	0.444	0.75 (0.66)	0.82
7	----		0.850 x 0.44	0.444	0.75 (0.68)	1.00

Table 1: Optimum Inline Orifice Configurations for MR = 2.0, S/H = 0.425, J = 36

* measured discharge coefficient

† y projection / S

effect on the mixing performance of inline configurations when a value of 2.55 was used for C in Eq. 1. The plates were designed for a MR of 2.0 when $J = 36$ and $S/H = 0.425$ in order to compare with those numerical results. However, the experimentally measured C_d for the plates was significantly less than the design point C_d . The lower C_d required $J = 48$ to achieve $MR = 2$.

Average jet mass fraction concentration distributions perpendicular to the mainstream flow direction for blockages of 0.59, 0.65, 0.81 and 0.89 are shown in Fig. 2a at 5 downstream positions starting at the trailing edge of each row of

orifices. The concentration distributions are plotted using 10 color-coded contours each representing a range in jet mass fraction of 0.1 from pure jet fluid = 1.0 (blue) to pure mainstream fluid = 0.0 (red). The fully mixed concentration of each configuration (c_{avg}) is 0.667.

In each configuration the jets penetrate to about 1/4 of the duct height, which has been shown to provide optimum mixing in an inline configuration². As the jets move downstream (top to bottom in fig. 2a) the distributions become similar, and at $x/H = 0.5$ the distributions appear equivalent.

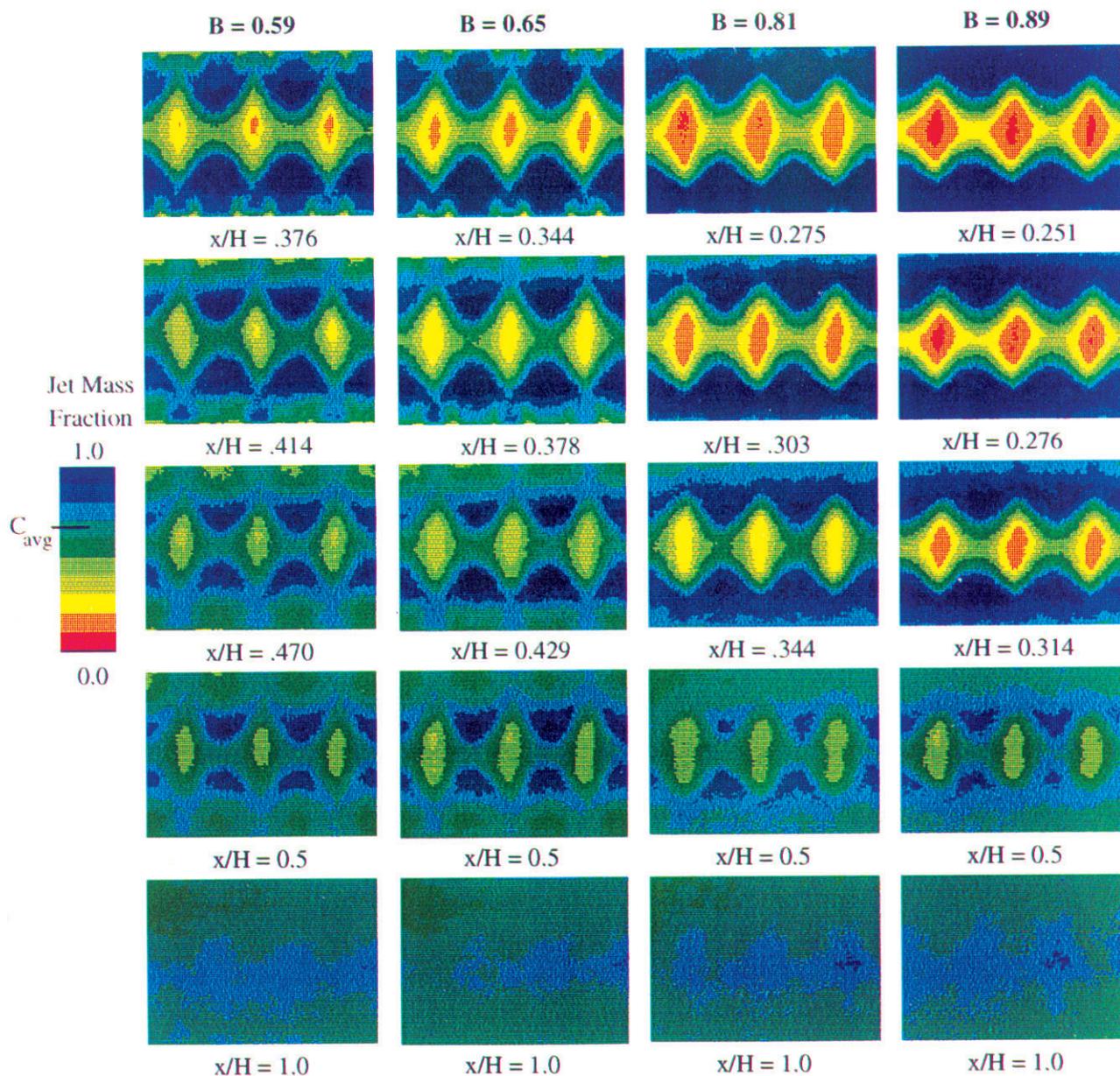


Figure 2a: Effect of Blockage on Opposed Inline Orifices at $MR = 2.0$, $S/H = 0.425$, $J = 48$

In fig. 2b average jet mass fraction concentration distributions are shown for a square ($B = 0.72$), a circle ($B = 0.82$), and a 2D slot ($B = 1.0$). The concentration distributions of the 2D slot indicate that the mainstream fluid remains in the center of the duct while the jet fluid stays near the walls. The mixing rate of this configuration appears lower than the cases where $B < 1.0$. At $x/H = 0.5$ the distributions of the rectangular and circular configurations appear similar to each other and to the corresponding distributions in Fig. 2a.

Spatial unmixedness is plotted as a function of downstream position (x/H) for the 7 configurations in Fig. 3. The curves are similar for all configurations except the 2D slot, which is consistently less mixed as a function of x/H . The surprising result is that mixing is independent of B over a range of 0.59 to 0.89. Similar performance independent of B can probably be attributed to the fact that the effective aerodynamic blockage is significantly less than the geometric blockage because of the vena contracta of the jet. For example, plate 3 has a blockage of 0.72 based on physical dimensions.

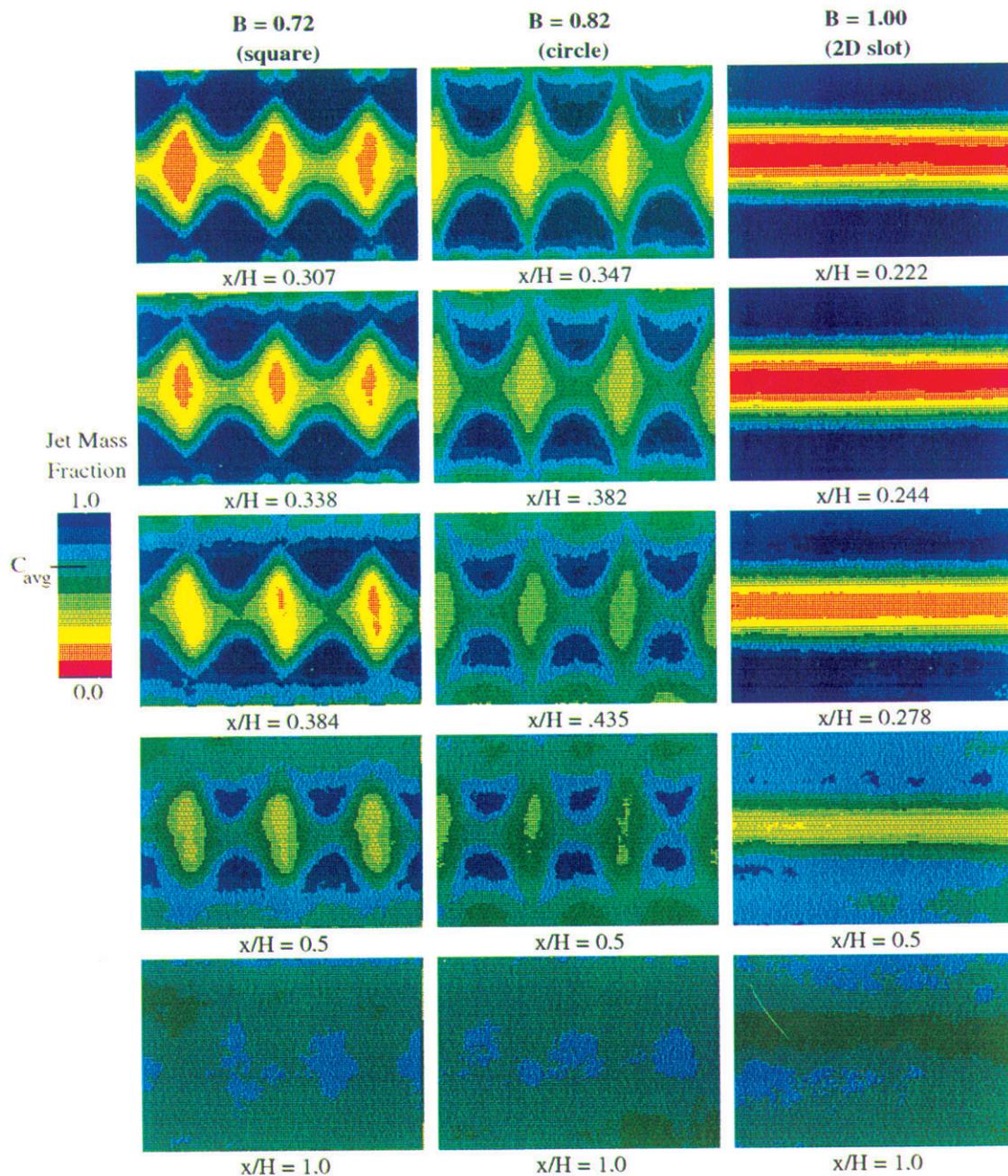


Figure 2b: Effect of Blockage on Opposed Inline Orifices at $MR = 2.0$, $S/H = 0.425$, $J = 48$

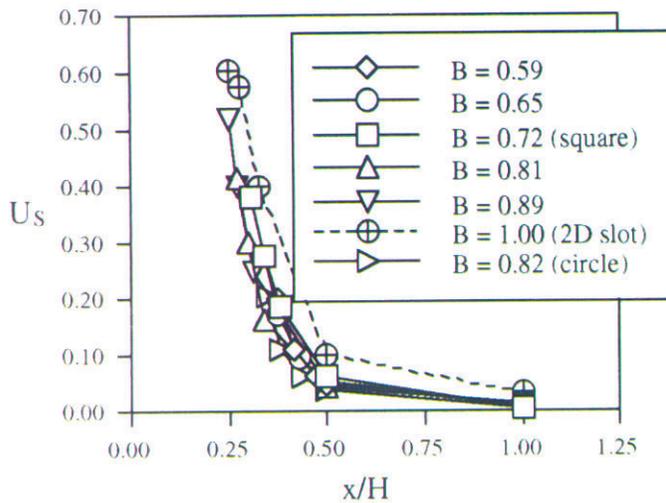


Figure 3: Effect of Blockage on Spatial Unmixedness at MR = 2.0, S/H = 0.425, J = 48

but only 0.58 when C_d is considered. Therefore even a configuration such as plate 5 that has a B of 0.89 allows a significant proportion of the mainstream to pass between adjacent jets due to the vena contracta of the orifice. The shear created by mainflow passing between the jets is necessary for development of a 3D flowfield which promotes mixing. The importance of the interplay between the jets and mainstream is evident from the concentration distribution of the 2D slot which confines the mainstream to the center of the duct.

As a practical design issue, the results indicate that web thickness can be set by mechanical constraints and not aerodynamics associated with mixing performance. Eq. 1 can be used without concern for a decrease in performance due to high B. The rate of mass addition as a function of downstream distance can therefore be increased by reduction of web thickness so that the axial length of the orifice can be minimized. Furthermore, circular and rectangularly shaped orifices with aspect ratios between 1-to-1 and 1-to-1.5 in both bluff and aligned orientations have similar levels of U_s at $x/H = 0.5$, but note that the bluff orientation offers the characteristic of smaller x projection per unit area.

Experimental and Numerical Results

A comparison of the experimental and numerical² jet mass fraction concentration distributions for the square orifice configuration (plate 3 in Table 1) is shown in Fig. 4 at the trailing edge of the orifice and at $x/H = 0.5$. In each case $S/H = 0.425$ and $J = 36$. C_{avg} for both distributions falls within the 7th contour (the experimental MR was 1.7 ($c_{avg} = 0.63$) compared to the numerical MR of 2.0 ($c_{avg} = 0.67$)). At each of the downstream locations the number of contours and jet penetration are in agreement. Unmixedness of the two cases is compared in Fig. 5. Good agreement is obtained at $x/H \geq 0.5$, but note that upstream of this location the curves appear to diverge.

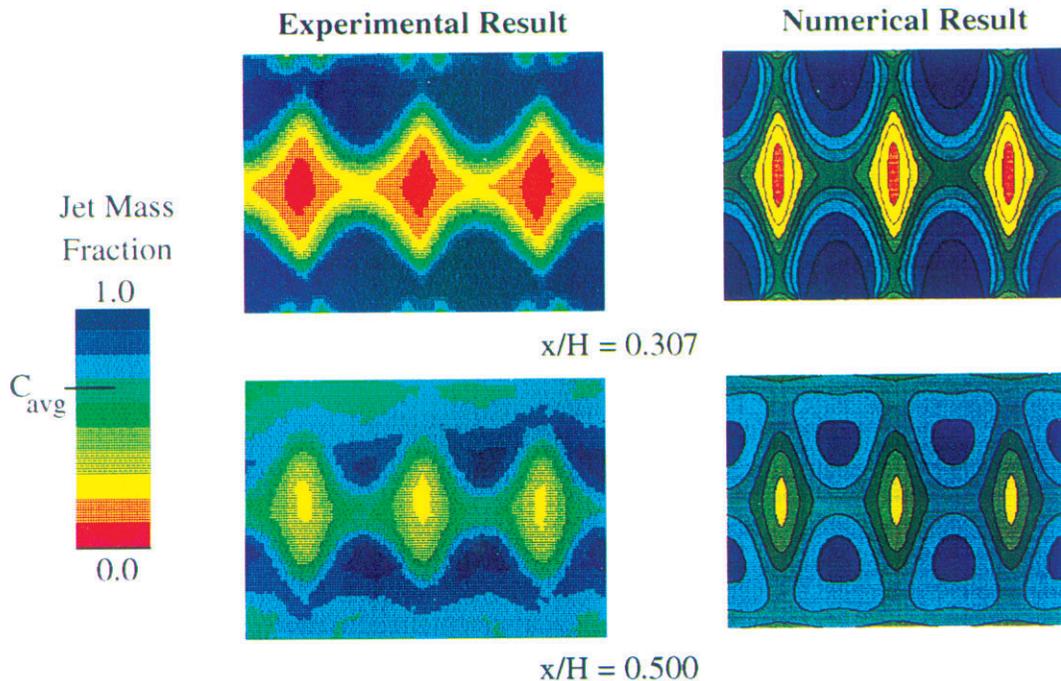


Figure 4: Concentration Distributions for a Square Orifice Configuration (Plate 3, Table 1) at S/H = 0.425, J = 36

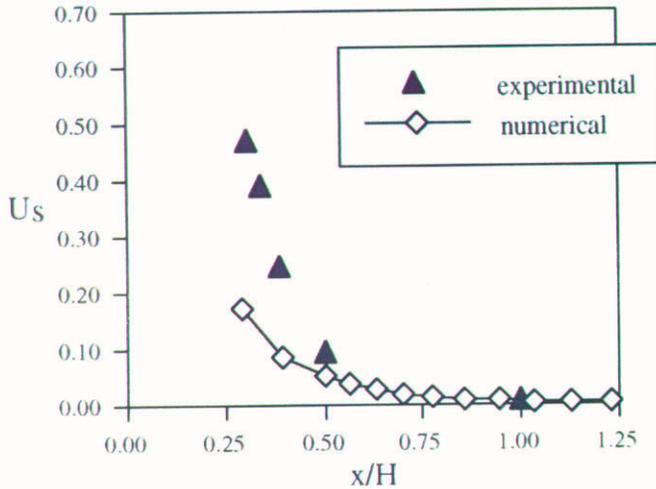


Figure 5: Comparison of Spatial Unmixedness for a Square Orifice Configuration (Plate 3 in Table 1) at $J = 36$ and $S/H = 0.425$

Effect of Orifice Shape

Crossflow jet mixing performance is directly related to jet penetration with optimum mixing for inline configurations occurring when the asymptotic mean trajectory is at $H/4^2$. Previous studies^{8 & 12} of a slot with an aspect ratio (long-to-short) > 2 have shown that jet penetration may be a function of orifice angle. Therefore in addition to orifice spacing, slot angle can be used to modify jet penetration. The characteristics of inline 45° slanted slots (aspect ratio 4:1) and round holes were investigated to show the effect of orifice shape on mixing.

Drawings of the two configurations and their corresponding concentration distributions at $x/H = 0.5$ are shown in Fig. 6. The orifices are equal in area, however the round orifice spacing was decreased to reduce jet penetration so that it was equal to that of the slanted slot case. In each case the jets penetrate to about $1/4$ of the duct height and mixing is similar as indicated by the comparable values of U_s shown in Fig. 7. Although orifice shape modifies the jet concentration distribution in the vicinity of injection, downstream mixing appears to be independent of shape for slanted slots and round holes, if aerodynamically equivalent cases are compared.

The results are presented to show that equivalent mean concentration distributions are not obtained at equal spacing for equal J . Therefore conclusions about the effect of orifice shape on multiple jet configurations can only be made from comparison of optimized configurations.

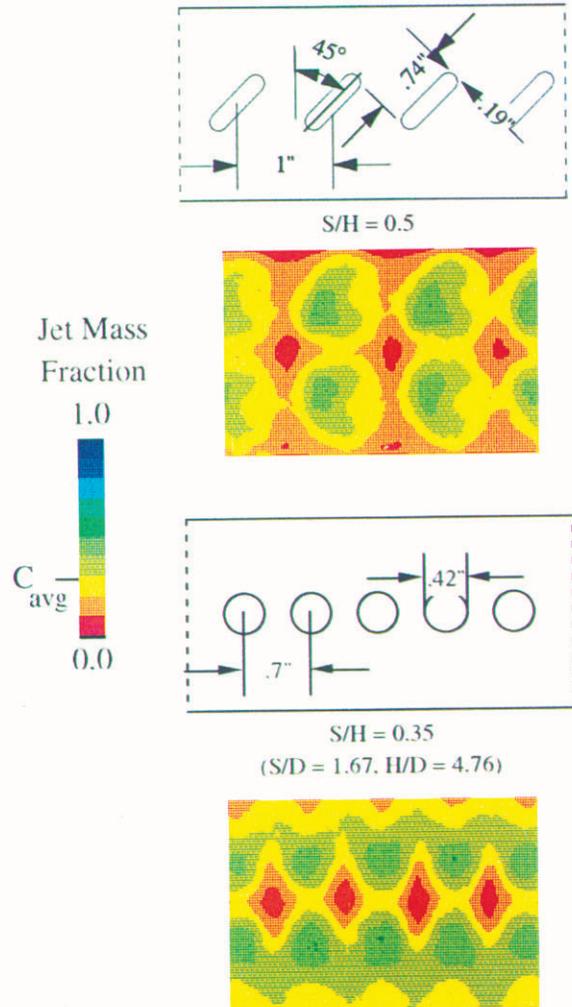


Figure 6: Orifice Configurations and Concentration Distributions for 45° 4:1 slots and Round Holes at $x/H = 0.5$ and $J = 25$

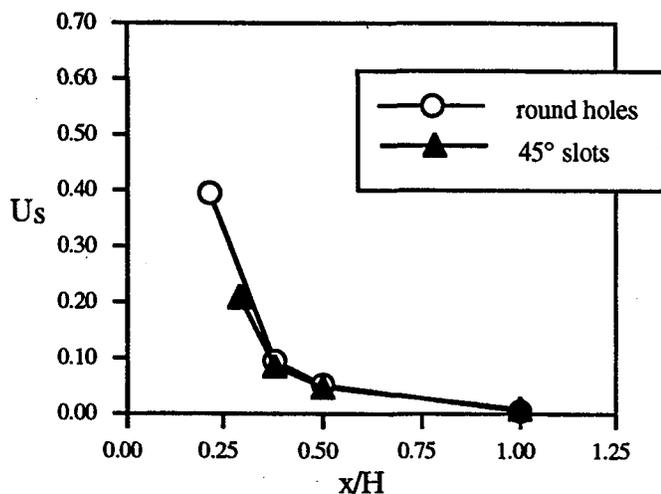


Figure 7: Comparison of Spatial Unmixedness for Equivalent 45° Slot and Round Hole Configurations at $J = 25$

Effect of Unequal Opposed Values of J

Annular combustors typically have an equal number of orifices on the ID and OD walls. Therefore in addition to an OD web that is larger than the ID web the local MR varies radially. The use of different diameter (and/or number) of orifices on the opposing walls may be considered to circumferentially distribute the jet fluid more uniformly. A design with different ID/OD jet areas might result in different ID/OD values for J.

The effect of varying opposing J values is compared to results of an empirical study¹⁹ in Fig. 8. In this experiment the orifice plate configuration was constant: $D = 0.25$ and $S/H = 0.25$ while the opposing J values were varied to maintain a constant MR of 0.325. This orifice configuration was found to be an optimum inline configuration when opposing values of J were equal and also an optimum configuration for single sided injection at the same MR. The concentration distributions vary as expected in that jet penetration is proportional to J. The values of U_s at $x/H = 0.5$ was about 0.03 for all cases although the circumferential profiles are distinctly different. The experimental and empirical results are in good agreement.

Conclusions

1. Compared at $x/H = 0.5$, orifice configurations with blockages ranging from 0.59 to 0.89 had similar mixing performance.
2. The design correlation for inline configurations at $MR = 2, 2.5 \approx (S/H)\sqrt{J}$, is independent of the web between adjacent orifices.
3. Numerical and experimental results were in good agreement for an orifice with aspect ratio of 1-to-1.
4. Conclusions about the performance of various orifice shapes can only be obtained from comparison of optimized configurations.
5. Experimental and empirical results were in good agreement for jets with different momentum-flux ratios on opposite sides.

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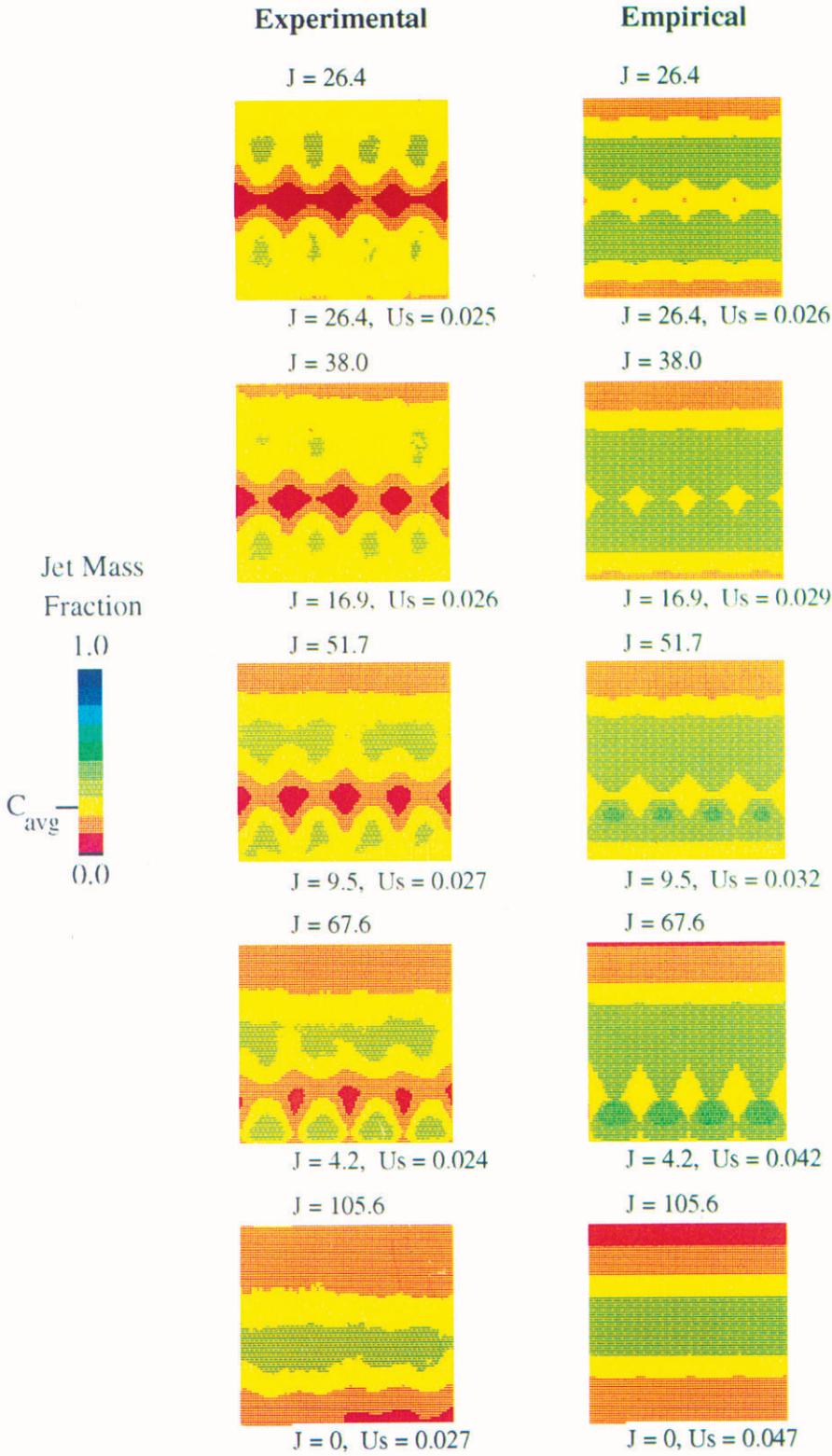


Figure 8: Comparison of Experimental and Empirical Results for Inline Round Orifices when Opposing J Values are Unequal ($S/H = 0.25$ and $x/H = 0.5$)

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13. ABSTRACT (<i>Maximum 200 words</i>) An experimental investigation of the mixing of nonreacting opposed rows of inline jets injected perpendicular to a uniform crossflow has been conducted in a rectangular duct. Planar Mie-scattering was used to measure the time-average concentration distribution of the jet fluid in planes perpendicular to the duct axis. Orifice configurations with geometric blockages ranging from 0.59 to 0.89 had similar mixing performance when compared at one-half duct height downstream of injection. Blockage was varied by changing the orifice aspect ratio from 1-to-1 to 1-to-1.5 while maintaining orifice spacing-to-duct height (S/H) at 0.425, jet-to-mainstream mass flow ratio (MR) at 2.0, and jet-to-mainstream momentum-flux ratio (J) at 48. The result indicates that the design correlating expression (at MR = 2) for optimum inline mixing of $2.5 \approx (S/H)\sqrt{J}$ is independent of the web between adjacent orifices and therefore independent of orifice width. Experimental and numerical results for an orifice aspect ratio 1-to-1 case were in good agreement. The results of a comparison of inline 45° slanted slot and round orifice configuration indicate that in order to obtain equivalent mean concentration distributions at the same J it is necessary to use a smaller S/H for the round orifice configuration. Conclusions about the performance of various orifice shapes can only be obtained from comparison of optimized configurations. Inline jets with different momentum-flux ratios on opposite sides were compared at a constant mass flow ratio. The orifice spacing chooser was previously found to be an optimum configuration when opposing values of J were equal and also an optimum for single side injection. Experimental and empirical results were in good agreement.			
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